

The Consumer Guide to Ultrasonic Flowmeters

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Seminar Outline

- **Introduction**
- *Fluid Flow Fundamentals*
- *Flowmeter Technology*
- *Flowmeter Performance*
- *Consumer Guide*

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Introduction

- *Working Definition of a Process*
- *Why Measure Flow?*

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Working Definition of a Process

- *A process is anything that changes*

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Why Measure Flow?

- *Flow measurements provide information about the process*
- *The information that is needed depends on the process*

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Why Measure Flow?

- *Custody transfer*
 - *Measurements are often required to determine the total quantity of fluid that passed through the flowmeter for billing purposes*

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Why Measure Flow?

- *Monitor the process*
 - *Flow measurements can be used to ensure that the process is operating satisfactorily*

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Why Measure Flow?

- *Improve the process*
 - *Flow measurements can be used for heat and material balance calculations that can be used to improve the process*

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Why Measure Flow?

- *Monitor a safety parameter*
 - *Flow measurements can be used to ensure that critical portions of the process operate safely*

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- *Flowmeter Technology*
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Fluid Flow Fundamentals

- ***Temperature***
- *Pressure*
- *Density and Fluid Expansion*
- *Types of Flow*
- *Inside Pipe Diameter*
- *Viscosity*
- *Reynolds Number and Velocity Profile*
- *Hydraulic Phenomena*



Temperature

- *Measure of relative hotness/coldness*
 - *Water freezes at 0°C (32°F)*
 - *Water boils at 100°C (212°F)*



Temperature

- *Removing heat from fluid lowers temperature*
 - *If all heat is removed, absolute zero temperature is reached at approximately -273°C (-460°F)*

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Temperature

- *Absolute temperature scales are relative to absolute zero temperature*
 - *Absolute zero temperature = 0 K (0°R)*
 - *Kelvin = $^{\circ}\text{C} + 273$*
 - *Rankin = $^{\circ}\text{F} + 460$*

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Temperature

- *Absolute temperature is important for flow measurement*

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Temperature

373 K = 100°C

273 K = 0°C

0 K = -273°C

672°R = 212°F

460°R = 0°F

0°R = -460°F

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Temperature

Problem

- *The temperature of a process increases from 20°C to 60°C. For the purposes of flow measurement, by what percentage has the temperature increased?*

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Temperature

- *It is tempting to answer that the temperature tripled (60/20), but the ratio of the absolute temperatures is important for flow measurement*
 - $(60+273)/(20+273) = 1.137$
 - 13.7% increase

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Fluid Flow Fundamentals

- *Temperature*
- **Pressure**
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Pressure

- *Pressure is defined as the ratio of a force divided by the area over which it is exerted ($P=F/A$)*

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Pressure

Problem

- *What is the pressure exerted on a table by a 2 inch cube weighing 5 pounds?*
 - $(5 \text{ lb}) / (4 \text{ inch}^2) = 1.25 \text{ lb/in}^2$
 - *If the cube were balanced on a 0.1 inch diameter rod, the pressure on the table would be 636 lb/in²*

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Pressure

- *Atmospheric pressure is caused by the force exerted by the atmosphere on the surface of the earth*
 - *2.31 feet WC / psi*
 - *10.2 meters WC / bar*

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Pressure

- *Removing gas from a container lowers the pressure in the container*
 - *If all gas is removed, absolute zero pressure (full vacuum) is reached at approximately -1.01325 bar (-14.696 psig)*

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Pressure

- *Absolute pressure scales are relative to absolute zero pressure*
 - *Absolute zero pressure*
 - *Full vacuum = 0 bar abs (0 psia)*
 - *bar abs = bar + 1.01325*
 - *psia = psig + 14.696*

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Pressure

The diagram illustrates the relationship between different pressure measurement scales. A horizontal line represents the 'Atmosphere' level. Below it, a dashed line indicates the 'Vacuum' scale, with an upward arrow. Above the 'Atmosphere' line, an upward arrow indicates the 'Absolute' scale. A double-headed vertical arrow between the 'Atmosphere' and 'Absolute' lines is labeled 'Differential'. To the right of the 'Atmosphere' line, another upward arrow indicates the 'Gauge' scale. The bottom-most horizontal line is labeled 'Absolute Zero'.

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Pressure

- *Absolute pressure is important for flow measurement*

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Pressure

Problem

- *The pressure of a process increases from 1 bar to 3 bar. For the purposes of flow measurement, by what percentage has the pressure increased?*

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Pressure

- *It is tempting to answer that the pressure tripled (3/1), but the ratio of the absolute pressures is important for flow measurement*
 - $(3+1.01325)/(1+1.01325) = 1.993$
 - 99.3% increase

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Fluid Flow Fundamentals

- *Temperature*
- *Pressure*
- ***Density and Fluid Expansion***
- *Types of Flow*
- *Inside Pipe Diameter*
- *Viscosity*
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Density and Fluid Expansion

- *Density is defined as the ratio of the mass of a fluid divided its volume*
($\rho = m/V$)

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Density and Fluid Expansion

- *Specific Gravity of a liquid is the ratio of its operating density to that of water at standard conditions*
 - $SG = \rho_{\text{liquid}} / \rho_{\text{water at standard conditions}}$

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Density and Fluid Expansion

Problem

- *What is the density of air in a 3.2 ft³ filled cylinder that has a weight of 28.2 and 32.4 pounds before and after filling respectively?*

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Density and Fluid Expansion

- *The weight of the air in the empty cylinder is taken into account*
 - $Mass = (32.4 - 28.2) + (3.2 \cdot 0.075)$
 $= 4.44 \text{ lb}$
 - $Volume = 3.2 \text{ ft}^3$
 - $Density = 4.44 / 3.2 = 1.39 \text{ lb/ft}^3$

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Density and Fluid Expansion

- *The density of most liquids is nearly unaffected by pressure*
- *Expansion of liquids*
 - $V = V_0 (1 + \beta \cdot \Delta T)$
 - V = new volume
 - V_0 = old volume
 - β = cubical coefficient of expansion
 - ΔT = temperature change

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Density and Fluid Expansion

Problem

- *What is the change in density of a liquid caused by a 10°C temperature rise where β is 0.0009 per °C ?*

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Density and Fluid Expansion

- *Calculate the new volume*
 - $V = V_0 (1 + 0.0009 \cdot 10) = 1.009 V_0$
 - *The volume of the liquid increased to 1.009 times the old volume, so the new density is (1/1.009) or 0.991 times the old density*

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Density and Fluid Expansion

- Expansion of solids
 - $V = V_0 (1 + \beta \cdot \Delta T)$
 - where $\beta = 3 \cdot \alpha$
 - α = linear coefficient of expansion
- Temperature coefficient
 - Stainless steel temperature coefficient is approximately 0.5% per 100°C

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Density and Fluid Expansion

Problem

- What is the increase in size of metal caused by a 50°C temperature rise where the metal has a temperature coefficient of 0.5% per 100°C?

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Density and Fluid Expansion

- Calculate the change in size
 - $(0.5 \cdot 50) = 0.25\%$
 - Metals (such as stainless steel) can exhibit significant expansion

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Density and Fluid Expansion

- Boyle's Law states the the volume of an ideal gas at constant temperature varies inversely with absolute pressure
 - $V = K / P$

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Density and Fluid Expansion

- New volume can be calculated
 - $V = K / P$
 - $V_0 = K / P_0$
- Dividing one equation by the other yields
 - $V/V_0 = P_0 / P$

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Density and Fluid Expansion

Problem

- How is the volume of an ideal gas at constant temperature and a pressure of 28 psig affected by a 5 psig pressure increase?

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Density and Fluid Expansion

- Calculate the new volume

- $V/V_0 = (28+14.7) / (28+5+14.7) = 0.895$

- $V = 0.895 V_0$

- Volume decreased by 10.5%

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Density and Fluid Expansion

- Charles' Law states the the volume of an ideal gas at constant pressure varies directly with absolute temperature

- $V = K \cdot T$

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Density and Fluid Expansion

- New volume can be calculated

- $V = K \cdot T$

- $V_0 = K \cdot T_0$

- Dividing one equation by the other yields

- $V/V_0 = T/T_0$

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Density and Fluid Expansion

Problem

- How is the volume of an ideal gas at constant pressure and a temperature of 15°C affected by a 10°C decrease in temperature?

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Density and Fluid Expansion

- Calculate the new volume
 - $V/V_0 = (273+15-10) / (273+15) = 0.965$
 - $V = 0.965 V_0$
 - Volume decreased by 3.5%

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Density and Fluid Expansion

- Ideal Gas Law combines Boyle's and Charles' Laws
 - $PV = nRT$

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Density and Fluid Expansion

- *New volume can be calculated*
 - $P \cdot V = n \cdot R \cdot T$
 - $P_0 \cdot V_0 = n \cdot R \cdot T_0$
- *Dividing one equation by the other yields*
 - $V/V_0 = (P_0/P) \cdot (T/T_0)$

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Density and Fluid Expansion

Problem

- *How is the volume of an ideal gas at affected by a 10.5% decrease in volume due to temperature and a 3.5% decrease in volume due to pressure?*

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Density and Fluid Expansion

- *Calculate the new volume*
 - $V/V_0 = 0.895 \cdot 0.965 = 0.864$
 - $V = 0.864 V_0$
 - *Volume decreased by 13.6%*

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Density and Fluid Expansion

- *Non-Ideal Gas Law takes into account non-ideal behavior*
 - $PV = nRTZ$

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Density and Fluid Expansion

- *New volume can be calculated*
 - $P \cdot V = n \cdot R \cdot T \cdot Z$
 - $P_0 \cdot V_0 = n \cdot R \cdot T_0 \cdot Z_0$
- *Dividing one equation by the other yields*
 - $V/V_0 = (P_0/P) \cdot (T/T_0) \cdot (Z/Z_0)$

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Fluid Flow Fundamentals

- *Temperature*
- *Pressure*
- *Density and Fluid Expansion*
- **Types of Flow**
- *Inside Pipe Diameter*
- *Viscosity*
- *Reynolds Number and Velocity Profile*
- *Hydraulic Phenomena*

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Types of Flow

- $Q = A \cdot v$
 - Q is the volumetric flow rate
 - A is the cross-sectional area of the pipe
 - v is the average velocity of the fluid in the pipe

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Types of Flow

- Typical Volumetric Flow Units ($Q = A \cdot v$)
 - $ft^2 \cdot ft/sec = ft^3/sec$
 - $m^2 \cdot m/sec = m^3/sec$
 - gallons per minute (gpm)
 - liters per minute (lpm)
 - cubic centimeters per minute (ccm)

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Types of Flow

- $W = \rho \cdot Q$
 - W is the mass flow rate
 - ρ is the fluid density
 - Q is the volumetric flow rate

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Types of Flow

- *Typical Mass Flow Units ($W = \rho \cdot Q$)*
 - $lb/ft^3 \cdot ft^3/sec = lb/sec$
 - $kg/m^3 \cdot m^3/sec = kg/sec$
 - *standard cubic feet per minute (scfm)*
 - *standard liters per minute (slpm)*
 - *standard cubic centimeters per minute (sccm)*

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Types of Flow

- $Q = A \cdot v$
- $W = \rho \cdot Q$

- Q *volumetric flow rate*
- W *mass flow rate*
- v *fluid velocity*
- $\frac{1}{2} \rho v^2$ *inferential flow rate*

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Inside Pipe Diameter

- The *inside pipe diameter (ID)* is important for flow measurement
 - Pipes of the same size have the same outside diameter (OD)
 - Welding considerations
 - Pipe wall thickness, and hence its ID, is determined by its schedule

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Inside Pipe Diameter

- Pipe wall thickness increases with increasing pipe schedule
 - Schedule 40 pipes are considered “standard” wall thickness
 - Schedule 5 pipes have thin walls
 - Schedule 160 pipes have thick walls

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Inside Pipe Diameter

- Nominal pipe size
 - For pipe sizes 12-inch and smaller, the nominal pipe size is the approximate ID of a Schedule 40 pipe
 - For pipe sizes 14-inch and larger, the nominal pipe size is the OD of the pipe

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Viscosity

- *Viscosity is the ability of the fluid to flow over itself*
- *Units*
 - *cP, cSt*
 - *Saybolt Universal (at 100°F, 210 °F)*
 - *Saybolt Furol (at 122°F, 210 °F)*

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Viscosity

- *Viscosity can be highly temperature dependent*
 - *Water*
 - *Honey at 40°F, 80°F, and 120°F*
 - *Peanut butter*

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Velocity Profile and Reynolds Number

- *Reynolds number is the ratio of inertial forces to viscous forces in the flowing stream*
- $R_D = 3160 \cdot Q_{gpm} \cdot SG / (\mu_{cP} \cdot D_{in})$

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Velocity Profile and Reynolds Number

- *Reynolds number can be used as an indication of how the fluid is flowing in the pipe*
- *Flow regimes based on R_D*
 - *Laminar* < 2000
 - *Transitional* 2000 - 4000
 - *Turbulent* > 4000

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Velocity Profile and Reynolds Number

- *Not all molecules in the pipe flow at the same velocity*
- *Molecules near the pipe wall move slower; molecules in the center of the pipe move faster*

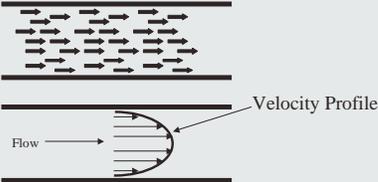
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Velocity Profile and Reynolds Number

- *Laminar Flow Regime*
 - *Molecules move straight down pipe*



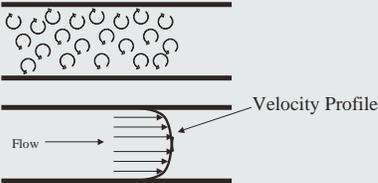
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Velocity Profile and Reynolds Number

- *Turbulent Flow Regime*
 - *Molecules migrate throughout pipe*



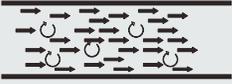
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Velocity Profile and Reynolds Number

- *Transitional Flow Regime*
 - *Molecules exhibit both laminar and turbulent behavior*

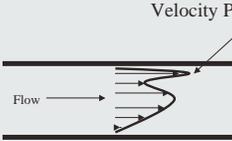


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Velocity Profile and Reynolds Number

- *Many flowmeters require a good velocity profile to operate accurately*
- *Obstructions in the piping system can distort the velocity profile*
 - *Elbows, tees, fittings, valves*

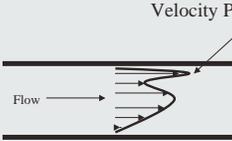


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Velocity Profile and Reynolds Number

- *A distorted velocity profile can introduce significant errors into the measurement of most flowmeters*



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Velocity Profile and Reynolds Number

- *Good velocity profiles can be developed*
 - *Straight run upstream and downstream*
 - *No fittings or valves*
 - *Upstream is usually longer and more important*
 - *Flow conditioner*
 - *Locate control valve downstream of flowmeter*

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Fluid Flow Fundamentals

- *Temperature*
- *Pressure*
- *Density and Fluid Expansion*
- *Types of Flow*
- *Inside Pipe Diameter*
- *Viscosity*
- *Reynolds Number and Velocity Profile*
- ***Hydraulic Phenomena***

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Hydraulic Phenomena

- *Vapor pressure is defined as the pressure at which a liquid and its vapor can exist in equilibrium*
 - *The vapor pressure of water at 100°C is atmospheric pressure (1.01325 bar abs) because water and steam can coexist*

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Hydraulic Phenomena

- *A saturated vapor is in equilibrium with its liquid at its vapor pressure*
 - *Saturated steam at atmospheric pressure is at a temperature of 100°C*

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Hydraulic Phenomena

- *A superheated vapor is a saturated vapor that is at a higher temperature than its saturation temperature*
 - *Steam at atmospheric pressure that is at 150°C is a superheated vapor with 50°C of superheat*

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Hydraulic Phenomena

- *Flashing is the formation of gas (bubbles) in a liquid after the pressure of the liquid falls below its vapor pressure*
 - *Reducing the pressure of water at 100°C below atmospheric pressure (say 0.7 bar abs) will cause the water to boil*

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Hydraulic Phenomena

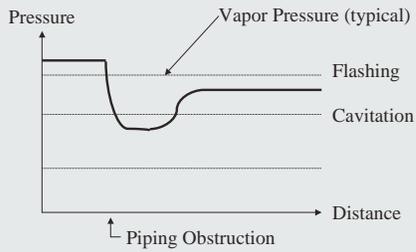
- *Cavitation is the formation and subsequent collapse of gas (bubbles) in a liquid after the pressure of the liquid falls below and then rises above its vapor pressure*
 - *Can cause severe damage in pumps and valves*

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Hydraulic Phenomena



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Hydraulic Phenomena

- *Energy Considerations*
 - *Claims are sometimes made that flowmeters with a lower pressure drop will save energy*

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Hydraulic Phenomena

- *Energy Considerations*

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Hydraulic Phenomena

- *Energy Considerations*

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Hydraulic Phenomena

- *Energy Considerations*

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Hydraulic Phenomena

- *Energy Considerations*

The graph plots Pressure (P) on the vertical axis and Flow (Q) on the horizontal axis. It shows three curves: a pump curve (decreasing pressure with increasing flow), a system curve (increasing pressure with increasing flow), and a combined curve for the system with a flowmeter and control valve (also increasing pressure with increasing flow, but higher than the system curve). The operating point is at flow rate Q and pressure P. A vertical dashed line at Q shows the pressure drop across the flowmeter and control valve as the difference between the system curve and the combined curve.

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Hydraulic Phenomena

- *Energy Considerations*

The graph is similar to slide 94, but the vertical distance between the system curve and the combined curve at flow rate Q is smaller, indicating a lower pressure drop across the flowmeter and control valve.

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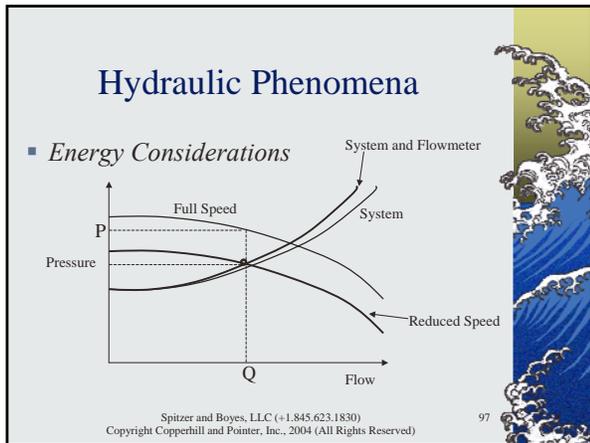
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Hydraulic Phenomena

- *Energy Considerations*
 - *The pump operates at the same flow and pressure, so no energy savings are achieved by installing a flowmeter with a lower pressure drop*

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- ## Hydraulic Phenomena
- *Energy Considerations*
- *Operating the pump at a reduced speed generates the same flow but requires a lower pump discharge pressure*
 - *Hydraulic energy generated by the pump better matches the load*
 - *Energy savings are proportional to the cube of the speed*
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- ## Seminar Outline
- *Introduction*
 - *Fluid Flow Fundamentals*
 - ***Flowmeter Technology***
 - *Flowmeter Performance*
 - *Consumer Guide*
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Ultrasonic Flowmeter Technology

- *Principle of Operation*
- *Path Geometry*
- *Correlation Designs*
- *Flowmeter Designs*
- *Transmitter Designs*
- *Installation*
- *Accessories*
- *Other Flowmeter Technologies*

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Principle of Operation

- *Ultrasonic flowmeters direct ultrasonic energy into the flowing stream*
- *Information from the remnants of this energy is used to determine the velocity of fluid passing through the flowmeter*

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Principle of Operation

- *Sensing the remnants is predicated upon a complete ultrasonic circuit*
 - *Transmitting device*
 - *Entry pipe wall (and liner)*
 - *Fluid (and reflections off pipe wall)*
 - *Exit pipe wall (and liner)*
 - *Receiving device*

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Principle of Operation

- *To function properly, all parts of the ultrasonic circuit must allow sufficient energy to pass*

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Principle of Operation

- *Weak signals may cause the flowmeter to be erratic or cease to function*
 - *Paint*
 - *Dry ultrasonic coupling compound*
 - *Pipe wall coating or corrosion*
 - *Poorly bonded liner*
 - *Tuberculation (barnacles)*

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Principle of Operation

- *Ultrasonic noise may cause the flowmeter to be erratic or cease to function*
 - *Nearby radio transmitter*
 - *Control valve with "quiet" trim*

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Principle of Operation Doppler Ultrasonic

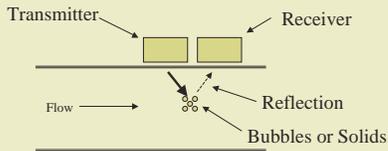
- *Doppler ultrasonic flowmeters reflect ultrasonic energy from particles, bubbles and/or eddies flowing in the fluid*

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Principle of Operation Doppler Ultrasonic



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Principle of Operation Doppler Ultrasonic

- *Under no flow conditions, the frequencies of the ultrasonic beam and its reflection are the same*
- *With flow in the pipe, the difference between the frequency of the beam and its reflection increases proportional to fluid velocity*

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Principle of Operation Doppler Ultrasonic

- *Doppler Equation*

$$v_f = K \cdot \Delta f$$

- K = constant
- v_f = velocity of fluid where ultrasonic energy is reflected
- Δf = difference between the transmitted and reflected frequencies

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Principle of Operation Transit Time Ultrasonic

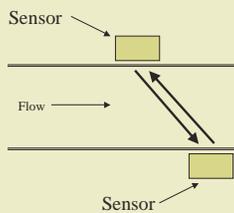
- *Transit time (time-of-flight) ultrasonic flowmeters alternately transmit ultrasonic energy into the fluid in the direction and against the direction of flow*

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Principle of Operation Transit Time Ultrasonic



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Principle of Operation Transit Time Ultrasonic

- *The time difference between ultrasonic energy moving upstream and downstream in the fluid is used to determine fluid velocity*

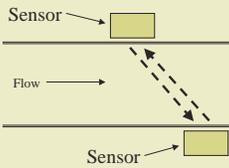
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Principle of Operation Transit Time Ultrasonic

- *Under no flow conditions, the time for the ultrasonic energy to travel upstream and downstream are the same*



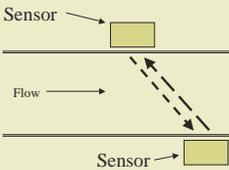
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Principle of Operation Transit Time Ultrasonic

- *With flow in the pipe, the time for the ultrasonic energy to travel upstream will be greater than the downstream time*



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Principle of Operation Transit Time Ultrasonic

- *Transit Time Equation*

$$v_p = \frac{K \cdot (T_u - T_d)}{T_u \cdot T_d}$$

- v_p = average fluid velocity in the path
- K = constant
- T_u = upstream transit time in fluid
- T_d = downstream transit time in fluid

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Principle of Operation Transit Time Ultrasonic

- T_u and T_d are dependent upon the speed of sound in the fluid
- Some designs use measurements and equations that are not dependent upon the speed of sound in the fluid

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Principle of Operation Pulse Repetition Ultrasonic

- *Pulse repetition (sing-around) ultrasonic flowmeters alternately transmit ultrasonic energy into the fluid in the direction and against the direction of flow*
- *The receipt of one ultrasonic pulse triggers the sending of a new ultrasonic pulse*

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Principle of Operation Pulse Repetition Ultrasonic

- *The frequency that the pulses are repeated is used to determine fluid velocity*

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Principle of Operation Pulse Repetition Ultrasonic

- *Pulse Repetition Equation*

$$v_p = K \cdot (f_u - f_d)$$

- v_p = average fluid velocity in the path
- K = constant
- f_u = frequency of upstream transit time period
- f_d = frequency of downstream transit time period

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Principle of Operation Phase Shift Ultrasonic

- *Phase shift ultrasonic flowmeters measure the phase shift between two continuous cyclic ultrasonic signals traveling in the direction and against the direction of flow*

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Principle of Operation Phase Shift Ultrasonic

- *Phase Shift Equation (constant frequency)*

$$v_p = \frac{K \bullet (\gamma_u - \gamma_d)}{\gamma_u \bullet \gamma_d}$$
 - v_p = average fluid velocity in the path
 - K = constant
 - γ_u = upstream phase angle
 - γ_d = downstream phase angle

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Principle of Operation Phase Shift Ultrasonic

- *Phase Shift Equation (varying frequency)*

$$v_p = \frac{K \bullet (f_u - f_d)}{\frac{1}{2} (f_u + f_d)}$$
 - v_p = average fluid velocity in the path
 - K = constant
 - f_u = upstream frequency
 - f_d = downstream frequency

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Ultrasonic Flowmeter Technology

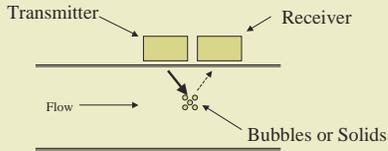
- *Principle of Operation*
- **Path Geometry**
- *Correlation Designs*
- *Flowmeter Designs*
- *Transmitter Designs*
- *Installation*
- *Accessories*
- *Other Flowmeter Technologies*

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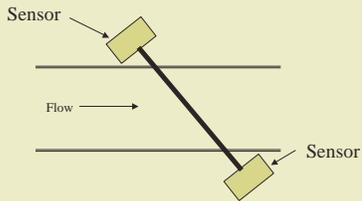
Doppler Path Geometry



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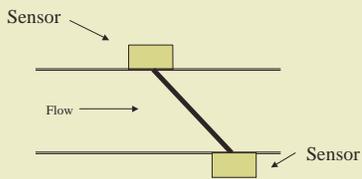
Single Path Geometry



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Single Path Geometry



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Single Path Geometry

One Reflection

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Single Path Geometry

Two Reflections

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Single Path Geometry

Three Reflections

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Single Path Geometry

Sensor → [] In Out [] ← Sensor

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Multiple Path Geometry

Sensor → []

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Chordal Path Geometry

Sensor → []

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Ultrasonic Flowmeter Technology

- *Principle of Operation*
- *Path Geometry*
- **Correlation Flowmeters**
- *Flowmeter Designs*
- *Transmitter Designs*
- *Installation*
- *Accessories*
- *Other Flowmeter Technologies*

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Correlation Flowmeters Principle of Operation

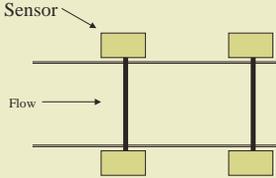
- *Correlation flowmeters determine fluid velocity by measuring parameters associated with the flowing stream at different places in the piping*

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Correlation Flowmeters Ultrasonic

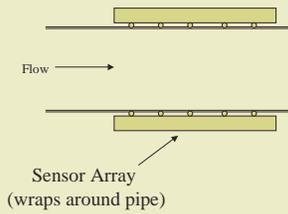


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Correlation Flowmeters Pressure Sensor Array



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Ultrasonic Flowmeter Technology

- *Principle of Operation*
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- *Transmitter Designs*
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- *Other Flowmeter Technologies*

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Ultrasonic Flowmeter Designs

- *Liquid*
 - *Portable and Handheld*
 - *Clamp-on*
 - *Spool*
 - *Probe (wetted)*
- *Gas, Stack Gas and Flare Gas*

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Ultrasonic Flowmeter Designs

- *Non-wetted design allows installation without shutting down flow*
 - *Portable and Handheld*
 - *Clamp-on*
- *Wetted design requires shutdown*
 - *Spool*
 - *Clamp-on spool*
 - *Probe (wetted)*

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Ultrasonic Flowmeter Technology

- *Principle of Operation*
- *Path Geometry*
- *Correlation Designs*
- *Flowmeter Designs*
- ***Transmitter Designs***
- *Installation*
- *Accessories*
- *Other Flowmeter Technologies*

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Ultrasonic Transmitter Designs

- *Analog*
 - *Electrical components subject to drift*
 - *Transit time more difficult to implement than Doppler*
 - *Mathematical corrections difficult*
 - *Four-wire design*

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Ultrasonic Transmitter Designs

- *Digital*
 - *Microprocessor is less susceptible to drift*
 - *Transit time algorithms easier to implement*
 - *Mathematical corrections in software*
 - *Four-wire design*
 - *Remote communication (with HART)*

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Ultrasonic Transmitter Designs

- *Fieldbus*
 - *Microprocessor is less susceptible to drift*
 - *Transit time algorithms easier to implement*
 - *Mathematical corrections in software*
 - *Multi-drop wiring*
 - *Remote communication*
 - *Issues with multiple protocols*

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Ultrasonic Flowmeter Technology

- *Principle of Operation*
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- *Flowmeter Designs*
- *Transmitter Designs*
- **Installation**
- *Accessories*
- *Other Flowmeter Technologies*

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Installation

- *Fluid Characteristics*
- *Piping and Hydraulics*
- *Ultrasonic Continuity*
- *Electrical*
- *Ambient Conditions*
- *Setup Information*

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Fluid Characteristics

- *Fluid must conduct ultrasonic energy*
 - *Water*
 - *Coal slurry*
 - *Low pressure gases (vacuum) can have few molecules*
- *Varying speed of sound in fluid*

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Fluid Characteristics

- *Within accurate flow range*
- *Corrosion and erosion*
- *Gas in liquid stream*
- *Immiscible fluids*

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Fluid Characteristics

- *Doppler*
 - *Typically requires 25-100 ppm of 25-100 micron bubbles or particles to reflect ultrasonic energy*
 - *Too many causes sensing at pipe wall*
 - *Too few may result in weak or non-representative reflection*

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Piping and Hydraulics

- *Keep flowmeter full of liquid*
 - *Hydraulic design*
 - *Vertical riser preferred*
 - *Avoid inverted U-tube*
 - *Be careful when flowing by gravity*

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Piping and Hydraulics

- *Maintain good velocity profile*
 - *Locate control valve downstream of flowmeter*
 - *Provide adequate straight run*
 - *Locate most straight run upstream*
 - *Install flow conditioner*
 - *Use full face gaskets*

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Piping and Hydraulics

- *Wetted parts compatible with fluid*
- *Pipe quality*
 - *Use smooth round pipe with known inside diameter, wall thickness, and material*
 - *Ultrasonic flowmeters measure velocity and infer volumetric flow assuming a known inside pipe diameter, wall thickness, and material*
 - *Spool design controls pipe quality*

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Piping and Hydraulics

- *Path length*
 - *Internal coating*
 - *Shortens path*
 - *Weakens reflections*
 - *Corrosion and erosion*
 - *Lengthens path*
 - *Distance between clamp-on transit time sensors must be accurate*
 - *Speed of sound in pipe*

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Piping and Hydraulics

- *Avoid piping configurations that could cause reflections of ultrasonic energy*
- *Avoid "low noise" valve trim*

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Ultrasonic Continuity

- *Clamp-on*
 - *Clean sensor/pipe interface - grease, paint*
 - *Conductive pipe material*
 - *Lining bonded to pipe*
 - *Lining material conductive*
 - *Conductive fluid*
 - *Clean reflective surfaces (multi-traverse)*

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Ultrasonic Continuity

- *Wetted sensors (probe)*
 - *Clean sensor/fluid interface*
 - *Conductive fluid*
 - *Clean reflective surfaces (multi-traverse)*

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Electrical

- *Integral sensors reduce wiring cost*
- *Avoid areas of electrical noise*
 - *AM radio stations*
 - *Variable speed drives*
- *Wiring*
 - *Low voltage power supply can eliminate power conduit*
 - *Fieldbus reduces wiring*

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Ambient Conditions

- *Outdoor applications (-20 to 60°C)*
 - *Many designs are for indoor locations*
- *Hazardous locations*
 - *Many designs are general purpose*

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Setup Information

- *GIGO (garbage in – garbage out)*
- *Entering correct information correctly is critical*
 - *Dimensions*
 - *Materials of construction*
 - *Fluid properties*

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Setup Information

- *Failure to use correct information can cause significant error and startup problems*

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Setup Information

Problem

- For a 6-inch pipe, what is the difference in diameter and area between schedule 40 and 80 pipe?

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Setup Information

- Both pipes are 6-inch, but the schedule 40 and 80 diameters are 6.065 and 5.761 inches respectively.
 - The diameters differ by approximately 5%
 - The cross-sectional areas differ by approximately 9%

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Ultrasonic Flowmeter Technology

- Principle of Operation
- Path Geometry
- Correlation Designs
- Flowmeter Designs
- Transmitter Designs
- Installation
- Accessories
- Other Flowmeter Technologies

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Accessories

- *Sensors*
 - *NEMA 4, 6P, and IP65, 67, 68*

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Accessories

- *Transmitter*
 - *NEMA 4X and IP65, 67*
 - *Analog output*
 - *Pulse output*
 - *Totalization and alarms*
 - *Data logging*
 - *HART, Foundation Fieldbus, Profibus*

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Ultrasonic Flowmeter Technology

- *Principle of Operation*
- *Path Geometry*
- *Correlation Designs*
- *Flowmeter Designs*
- *Transmitter Designs*
- *Installation*
- *Accessories*
- ***Other Flowmeter Technologies***

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Other Flowmeter Technologies

- *Coriolis Mass* *Insertion*
- *Differential Pressure*
- *Magnetic*
- *Positive Displacement*
- *Target*
- *Thermal*
- *Turbine*
- *Ultrasonic*
- *Vortex Shedding*

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Coriolis Mass Flowmeter

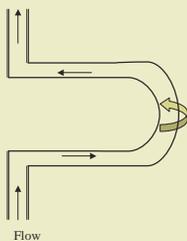
- *Coriolis mass flowmeters measure the force generated as the fluid moves towards/away from its center of rotation*

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Coriolis Mass Flowmeter



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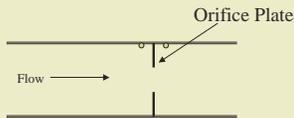
Differential Pressure Flowmeter

- *A piping restriction is used to develop a pressure drop that is measured and used to infer fluid flow*
 - *Primary Flow Element*
 - *Transmitter (differential pressure)*

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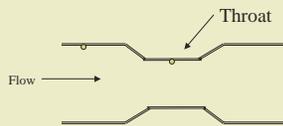
Orifice Plate Primary Flow Element



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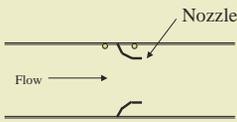
Venturi Primary Flow Element



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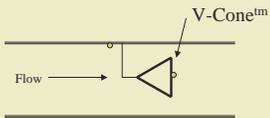
Flow Nozzle Primary Flow Element



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V-Cone™ Primary Flow Element



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Differential Pressure Flowmeter

- *Pressure drop is proportional to the square of the fluid flow rate*
 - $\Delta p \propto Q^2$ or $Q \propto \text{sqrt}(\Delta p)$
 - *Double the flow... four times the differential*

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Differential Pressure Flowmeter

- *Low flow measurement can be difficult*
 - *For example, only 1/4 of the differential pressure is generated at 50 percent of the full scale flow rate. At 10 percent flow, the signal is only 1 percent of the differential pressure at full scale.*

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Magnetic Flowmeter

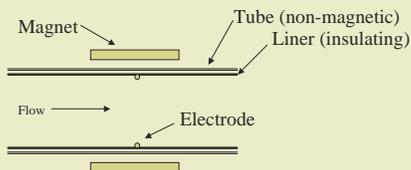
- *Fluid flow through a magnetic field generates a voltage at the electrodes that is proportional to fluid velocity*
 - *Primary Flow Element*
 - *Transmitter*

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Magnetic Flowmeter



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Magnetic Flowmeter

- *Traditional AC excitation was susceptible to noise and drift*
 - *A low voltage signal is generated that is susceptible to noise and cross-talk at the excitation frequency*

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Magnetic Flowmeter

- *Pulsed DC excitation reduces drift by turning the magnet on and off*
 - *Noise (while the magnet is off) is subtracted from signal and noise (while the magnet is on) to reduce the effects of noise and cross-talk*
 - *Response time can be compromised*

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Positive Displacement Flowmeter

- *Positive displacement flowmeters measure flow by repeatedly entrapping fluid within the flowmeter*
 - *Moving parts with tight tolerances*
 - *Bearings*
 - *Many shapes*

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Target Flowmeter

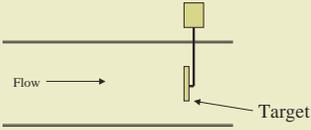
- *Target flowmeters determine flow by measuring the force exerted on a body (target) suspended in the flow stream*

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Target Flowmeter



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Thermal Flowmeter

- *Thermal flowmeters use the thermal properties of the fluid to measure flow*
 - *Hot Wire Anemometer*
 - *Thermal Profile*

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Thermal Flowmeter Hot Wire Anemometer

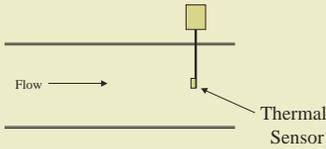
- *Hot wire anemometers determine flow by measuring the amount of energy needed to heat a probe whose heat loss changes with flow rate*

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Thermal Flowmeter Hot Wire Anemometer



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Thermal Flowmeter Thermal Profile

- *Thermal profile flowmeters determine flow by measuring the temperature difference that results in a heated tube when the fluid transfers heat from the upstream portion to the downstream portion of the flowmeter*

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Thermal Flowmeter Thermal Profile

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Turbine Flowmeter

- *Fluid flow causes a rotor to spin whereby the rotor speed is proportional to fluid velocity*
 - *Primary Flow Element*
 - *Transmitter*

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Turbine Flowmeter

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Turbine Flowmeter

- *The sensor detects the rotor blades*
- *The frequency of the rotor blades passing the sensor is proportional to fluid velocity*

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Ultrasonic - Doppler

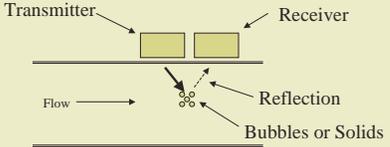
- *Doppler ultrasonic flowmeters reflect ultrasonic energy from particles, bubbles and/or eddies flowing in the fluid*

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Ultrasonic - Doppler



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Ultrasonic - Doppler

- *Under no flow conditions, the frequencies of the ultrasonic beam and its reflection are the same*
- *With flow in the pipe, the difference between the frequency of the beam and its reflection increases proportional to fluid velocity*

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Ultrasonic - Transit Time

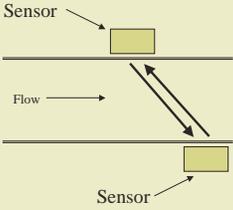
- *Transit time (time-of-flight) ultrasonic flowmeters alternately transmit ultrasonic energy into the fluid in the direction and against the direction of flow*

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Ultrasonic - Transit Time



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Ultrasonic - Transit Time

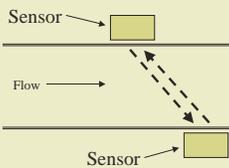
- *The time difference between ultrasonic energy moving upstream and downstream in the fluid is used to determine fluid velocity*

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Ultrasonic - Transit Time

- *Under no flow conditions, the time for the ultrasonic energy to travel upstream and downstream are the same*

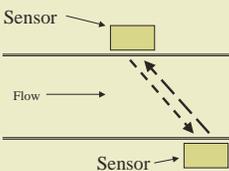


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Ultrasonic - Transit Time

- *With flow in the pipe, the time for the ultrasonic energy to travel upstream will be greater than the downstream time*



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Vortex Shedding Flowmeter

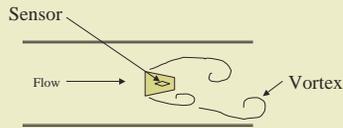
- *A bluff body in the flow stream creates vortices whereby the number of vortices is proportional to the fluid velocity*
 - *Primary Flow Element*
 - *Transmitter*

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Vortex Shedding Flowmeter



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Vortex Shedding Flowmeter

- *The sensing system detects the vortices created*
- *The frequency of the vortices passing the sensing system is proportional to fluid velocity*

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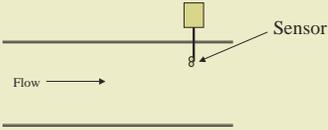
Insertion Flowmeter

- *Insertion flowmeter infer the flow in the entire pipe by measuring flow at one or more strategic locations in the pipe*
 - *Differential Pressure*
 - *Magnetic*
 - *Target*
 - *Thermal*
 - *Turbine*
 - *Vortex*

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Insertion Flowmeter



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Seminar Outline

- *Introduction*
- *Fluid Flow Fundamentals*
- *Flowmeter Technology*
- ***Flowmeter Performance***
- *Consumer Guide*

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Flowmeter Performance

- **Flowmeter Performance**
- *Performance Statements*
- *Reference Performance*
- *Pulse Output vs. Analog Output*
- *Actual Performance*
- *Supplier Claims*

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Flowmeter Performance

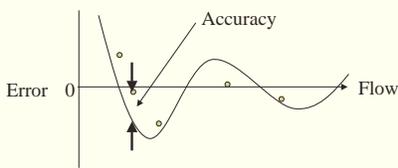
- *Accuracy is the ability of the flowmeter to produce a measurement that corresponds to its characteristic curve*

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Flowmeter Performance



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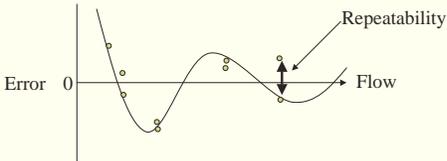
Flowmeter Performance

- *Repeatability is the ability of the flowmeter to reproduce a measurement each time a set of conditions is repeated*

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Flowmeter Performance



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Flowmeter Performance

- *Linearity is the ability of the relationship between flow and flowmeter output (often called the characteristic curve or signature of the flowmeter) to approximate a linear relationship*

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Flowmeter Performance

The graph plots Error on the vertical axis and Flow on the horizontal axis. A horizontal line at Error = 0 represents zero error. A wavy curve represents the actual flowmeter performance. A straight line is drawn through the curve, labeled 'Linearity', indicating the ideal linear relationship.

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Flowmeter Performance

- *Flowmeter suppliers often specify the composite accuracy that represents the combined effects of repeatability, linearity and accuracy*

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Flowmeter Performance

The graph plots Error on the vertical axis and Flow on the horizontal axis. A horizontal line at Error = 0 is shown. A wavy curve represents the flowmeter's performance. A straight line is drawn through the curve. A shaded area between the curve and the straight line is labeled 'Composite Accuracy (in Flow Range)'. A horizontal double-headed arrow at the bottom indicates the 'Flow Range' over which this accuracy is specified.

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Flowmeter Performance

- *Flowmeter Performance*
- **Performance Statements**
- *Reference Performance*
- *Pulse Output vs. Analog Output*
- *Actual Performance*
- *Supplier Claims*

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Performance Statements

- *Percent of rate*
- *Percent of full scale*
- *Percent of meter capacity (upper range limit)*
- *Percent of calibrated span*

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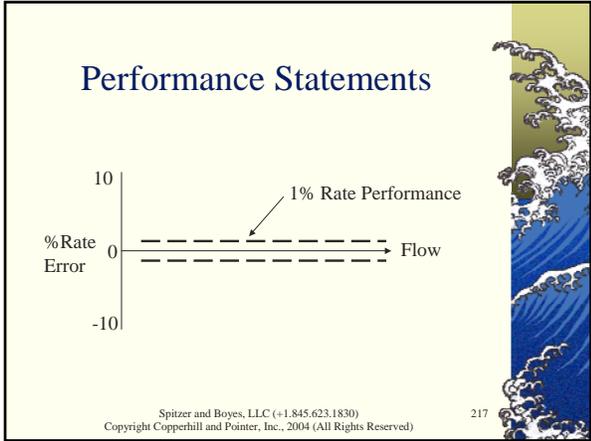
Performance Statements

- *1% of rate performance at different flow rates with a 0-100 unit flow range*
- *100% flow → 0.01•100 1.00 unit*
- *50% flow → 0.01•50 0.50 unit*
- *25% flow → 0.01•25 0.25 unit*
- *10% flow → 0.01•10 0.10 unit*

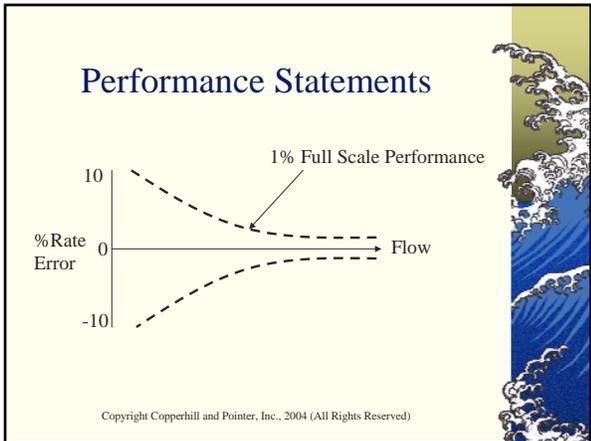
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- ### Performance Statements
- 1% of full scale performance at different flow rates with a 0-100 unit flow range
 - 100% flow $\rightarrow 0.01 \cdot 100$ 1 unit = 1% rate
 - 50% flow $\rightarrow 0.01 \cdot 100$ 1 unit = 2% rate
 - 25% flow $\rightarrow 0.01 \cdot 100$ 1 unit = 4% rate
 - 10% flow $\rightarrow 0.01 \cdot 100$ 1 unit = 10% rate
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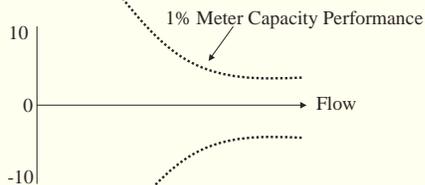
Performance Statements

- *1% of meter capacity (or upper range limit) performance at different flow rates with a 0-100 unit flow range (URL=400)*
 - *100% flow $\rightarrow 0.01 \cdot 400$ 4 units = 4% rate*
 - *50% flow $\rightarrow 0.01 \cdot 400$ 4 units = 8% rate*
 - *25% flow $\rightarrow 0.01 \cdot 400$ 4 units = 16% rate*
 - *10% flow $\rightarrow 0.01 \cdot 400$ 4 units = 40% rate*

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Performance Statements



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Performance Statements

- *Performance expressed as a percent of calibrated span is similar to full scale and meter capacity statements where the absolute error is a percentage of the calibrated span*

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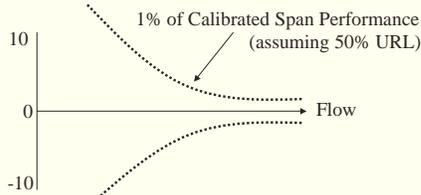
Performance Statements

- *1% of calibrated span performance at different flow rates with a 0-100 unit flow range (URL=400, calibrated span=200)*
 - *100% flow $\rightarrow 0.01 \cdot 200$ 2 units = 2% rate*
 - *50% flow $\rightarrow 0.01 \cdot 200$ 2 units = 4% rate*
 - *25% flow $\rightarrow 0.01 \cdot 200$ 2 units = 8% rate*
 - *10% flow $\rightarrow 0.01 \cdot 200$ 2 units = 20% rate*

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Performance Statements



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Performance Statements

- *A calibrated span statement becomes a full scale statement when the instrument is calibrated to full scale*
- *A calibrated span statement becomes a meter capacity statement when the instrument is calibrated at URL*

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Performance Statements

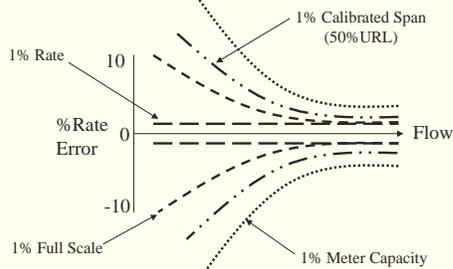
- *Performance specified as a percent of rate, percent of full scale, percent of meter capacity, and percent of calibrated span are different*

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Performance Statements



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Performance Statements

- *Different and multiple performance statements may apply*
 - *0.05% full scale typical transmitter*
 - *0.10% full scale low range transmitter*
 - *0.50% rate 50-100% full scale*
 - *0.25% full scale 10-50% full scale*

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Performance Statements

- *Performance statements apply over a range of operation*
- *Turndown is the ratio of the maximum flow that the flowmeter will measure within the stated accuracy to the minimum flow that can be measured within the stated accuracy*

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Performance Statements

- *Performance statements can be manipulated because their meaning may not be clearly understood*
- *Technical assistance may be needed to analyze the statements*

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Flowmeter Performance

- *Flowmeter Performance*
- *Performance Statements*
- **Reference Performance**
- *Pulse Output vs. Analog Output*
- *Actual Performance*
- *Supplier Claims*

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Reference Performance

- *Reference performance is the quality of measurement at a nominal set of operating conditions, such as:*
 - *Water at 20°C in ambient conditions of 20°C and 50 percent relative humidity*
 - *Long straight run*
 - *Pulse output*

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Reference Performance

- *In the context of the industrial world, reference performance reflects performance under controlled laboratory conditions*

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Reference Performance

- *Hypothetical flowmeter*
 - *1% rate 1-10 m/s*
 - *0.01 m/s 0.1-1 m/s*
 - *Undefined under 0.1 m/s*

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Reference Performance

Example - Omission

- *Hypothetical flowmeter*
 - 1% rate 10-100% of flow
 - 2% rate 5-10% of flow
- *Percent of flow could be assumed to be percent of user's full scale*

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Reference Performance

Example - Omission

- *If full scale is not adjustable, the percent is a percent of meter capacity!*
 - 0-100 unit range with URL=400 units
 - 1% rate 40-100 units
 - 2% rate 20-40 units

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Reference Performance

Example - Omission

- *Similarly, a percent of full scale statement could really be a percent of meter capacity statement*

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Reference Performance

Problem

- *If the full scale is not adjustable, what is the performance of a flowmeter with the following accuracy specifications?*
 - *1% full scale 10-100% flow*
 - *2% full scale 5-10% flow*

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Reference Performance

Solution

- *Ultrasonic flowmeters can operate upwards of 20 m/s*
 - *Assume meter capacity is 20 m/s*
- *In typical applications, fluid velocity is below 3 m/s*
 - *Assume a user range of 0-2 m/s*

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Reference Performance

Solution

- *The calculated accuracy is:*
 - *0.02*20 m/s 1-2 m/s*
 - *20% rate at 2 m/s*
 - *40% rate at 1 m/s*
 - *Undefined under 1 m/s*

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Reference Performance

- *Rate statements at high velocity are often discussed*
- *Errors at lower velocity are often only mentioned with prompting*
 - *Progressive disclosure*

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Flowmeter Performance

- *Flowmeter Performance*
- *Performance Statements*
- *Reference Performance*
- ***Pulse Output vs. Analog Output***
- *Actual Performance*
- *Supplier Claims*

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Pulse Output vs. Analog Output

- *Most suppliers specify pulse output performance*
 - *Analog output performance is typically the pulse output performance plus an absolute error*

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Pulse Output vs. Analog Output

Problem

- *What is the error associated with a 4-20mA analog output that has an error of 0.010 mA?*

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Pulse Output vs. Analog Output

Solution

- *The conversion error is:*
 - $0.010/(20-4) = 0.06\%$ of full scale
- *Many flowmeters have analog output errors of 0.10% of full scale*

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Pulse Output vs. Analog Output

Solution

<u>Flow</u>	<u>0.06% Full Scale</u>
100 units	$0.06 * 100 / 100 = 0.06\%$ rate
50 “	$0.06 * 100 / 50 = 0.12$ “
25 “	$0.06 * 100 / 25 = 0.24$ “
10 “	$0.06 * 100 / 10 = 0.60$ “

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Pulse Output vs. Analog Output

Solution

<i>Flow</i>	<i>0.10% Full Scale</i>
100 units	$0.10 * 100 / 100 = 0.10\%$ rate
50 “	$0.10 * 100 / 50 = 0.20$ “
25 “	$0.10 * 100 / 25 = 0.40$ “
10 “	$0.10 * 100 / 10 = 1.00$ “

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Pulse Output vs. Analog Output

- *Some suppliers cannot provide an analog output accuracy specification, so the performance of the analog output may be **undefined***

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Pulse Output vs. Analog Output

- *In some flowmeter designs, the analog output error can be **larger** than the flowmeter accuracy*
 - *Often applies to flowmeters with percent of rate accuracy*
 - *Rate error increases at low flow rates*
 - *Others often include the analog output error in their pulse accuracy statement*

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Pulse Output vs. Analog Output

- *Flowmeters with percent of full scale, meter capacity, and calibrated span often include the analog output error in their pulse accuracy statement*

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Pulse Output vs. Analog Output

Example

- *An analog output error of 0.10% of full scale is usually neglected for a flowmeter that exhibits 1% of full scale performance.*

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Flowmeter Performance

- *Flowmeter Performance*
- *Performance Statements*
- *Reference Performance*
- *Pulse Output vs. Analog Output*
- ***Actual Performance***
- *Supplier Claims*

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Actual Performance

- *Operating Effects*
 - *Ambient conditions*
 - *Humidity*
 - *Precipitation*
 - *Temperature*
 - *Direct sunlight*

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Actual Performance

- *Many flowmeters are rated to 10-90% relative humidity (non-condensing)*
 - *Outdoor locations are subject to 100% relative humidity and precipitation in various forms*

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Actual Performance

- *Operating Effects*
 - *Can be significant, even though the numbers seem small*
 - *Not published by most suppliers*
 - *Information is not generally available to fairly evaluate actual performance*

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Actual Performance

Example

- *The error (at 25 percent of scale and a 0°C ambient) associated with a temperature effect of 0.01% full scale per °C can be calculated as:*
 - $0.01 * (20-0) / 25$, or 0.80% rate

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Actual Performance

- *Pipe Size vs. Path Length*
 - *Large pipe sizes increase path length and transit time*
 - *Ultrasonic energy can limit path length/size*
 - *Relatively accurate time measurement*

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Actual Performance

- *Pipe Size vs. Path Length*
 - *Small pipe size decreases path length and transit time*
 - *Ultrasonic energy usually not a problem*
 - *Short path length decreases transit time and degrades time measurement (resolution issues)*

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Actual Performance

- *Pipe Size vs. Path Length*
 - *To increase the path length and transit time, many small ultrasonic flowmeters:*
 - *use a U-shaped axial path*
 - *reflect the ultrasonic energy off the inside wall of the pipe (one or more times)*

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Actual Performance

- *Velocity Profile*
 - *Distorted velocity profile can affect performance*
 - *Provide adequate straight run*
 - *Locate most of the straight run upstream of the flowmeter*

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Actual Performance

- *Velocity Profile*
 - *Distorted velocity profile can affect performance*
 - *Install a flow conditioner*
 - *Increase the number of paths*
 - *Alter the path location (chordal)*

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Actual Performance

- *Pipe Diameter and Area*
 - *For ultrasonic flowmeters, reference performance describes the quality of the velocity measurement*

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Actual Performance

- *Pipe Diameter and Area*
 - *Flow measurement (volume) is inferred from velocity measurement assuming*
 - *Good pipe condition*
 - *Known pipe wall thickness and material*
 - *Known pipe diameter, wall thickness, and area*

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Actual Performance

- *Pipe Diameter and Area*
 - *Variations in the condition of the pipe can affect the area of flow, points of reflection, and path length*

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Actual Performance

- *Pipe Diameter and Area*
 - *Variations in the pipe wall thickness and material can affect the compensation for the time that the ultrasonic energy travels in the pipe wall*

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Actual Performance

- *Pipe Diameter and Area*
 - *Variations in the pipe diameter, wall thickness, and area affect the calculations used to infer a flow measurement (volume) from the velocity measurement*

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Actual Performance

- *Pipe Diameter and Area*
 - *Ultrasonic flowmeters assume that the pipe diameter and wall thickness is known*
 - *Pipe diameter and wall thickness is not known for existing pipe, unmeasured pipe, and spools that are not wet tested*

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Actual Performance

- *Fluid Properties*
 - *Reference accuracy is determined using a known fluid at known conditions*

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Actual Performance

- *Fluid Properties*
 - *Variation from reference conditions may require calibration correlations that can affect flowmeter performance*
 - *Different fluid composition*
 - *Different fluid temperature*

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Flowmeter Performance

- *Flowmeter Performance*
- *Performance Statements*
- *Reference Performance*
- *Analog Output vs. Pulse Output*
- *Actual Performance*
- ***Supplier Claims***

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Supplier Claims

- *High Turndown*
 - *Example - Hypothetical flowmeter*
 - *1% rate accuracy*
 - *1000:1 turndown*
 - *Sounds fantastic!*

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Supplier Claims

- *High Turndown*
 - *Further investigation reveals*
 - *1% rate accuracy 0.5-10 m/s*
 - *0.005 m/s accuracy 0.01-0.5 m/s*
 - *Measures 0.01-10 m/s 1000:1 turndown*

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Supplier Claims

- *High Turndown*
 - *Performance expressed as a percent of rate degrades below 0.5 m/s*
 - *5% rate 0.10 m/s*
 - *10% rate 0.05 m/s*
 - *50% rate 0.01 m/s*

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Supplier Claims

- *Low Flow Operation*
 - *Flowmeter operates at low flows, but performance expressed as a percent of rate is degraded*
 - *5% rate 0.10 m/s*
 - *10% rate 0.05 m/s*
 - *50% rate 0.01 m/s*

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Supplier Claims

- *High Accuracy*
 - *High accuracy claims often refer to high flow rates that may not be practical*
 - *Often disguised by omission*
 - *“0.25% accuracy” (omits rate, full scale, meter capacity, calibrated span)*

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Supplier Claims

- *No Piping Obstructions*
 - *Most designs have no piping obstructions (especially clamp-on)*
 - *Some small designs are U-shaped*
 - *Wetted sensor designs can create a small void at the pipe wall*

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Supplier Claims

- *Clamp-on and Measure Flow*
 - *Claims often include*
 - *No pressure drop*
 - *No moving parts*
 - *No wetted parts, so no problems with materials of construction*
 - *Universal applicability*

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Supplier Claims

- *Clamp-on and Measure Flow*
 - *Common problems*
 - *Ultrasonic path needs to be complete (pipe, liner, fluid...)*
 - *Pipe diameter, wall thickness, and area uncertainty*
 - *Uncertain condition of pipe*
 - *Velocity profile*

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Supplier Claims

- *Clamp-on and Measure Flow*
 - *Transit time problems*
 - *Some designs are affected by speed of sound in the fluid*
 - *Sensor positioning (path length)*
 - *Pipe coating*

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Supplier Claims

- *Clamp-on and Measure Flow*
 - *Doppler problems*
 - *Needs particles and bubbles within size and concentration limits (difficult to control)*
 - *Ultrasonic energy may penetrate too deep or not deep enough*

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Supplier Claims

- *Reynolds Number Compensation*
 - *Reynolds number effects can be as high as 20% rate at low Reynolds numbers*
 - *Claims include*
 - *Some ultrasonic flowmeters compensate for Reynolds number*

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Supplier Claims

- *Reynolds Number Compensation*
 - *Problems include*
 - *Compensation is dependent upon programmed or inferred fluid properties (viscosity, density, pipe size...)*

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Supplier Claims

- *Chordal Path*
 - *Claims include*
 - *More accurate measurement by avoiding the high centerline velocity*

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Supplier Claims

- *Chordal Path*
 - *Claims include*
 - *Avoid inferring velocity profile from Reynolds number by determining the velocity profile from chordal and diametrical path measurements*

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Supplier Claims

- *Speed of Sound in Fluid*
 - *Claims include*
 - *Some designs use equations that are not affected by variations in the speed of sound in the fluid*

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Supplier Claims

- *Clamp-on Angle of Refraction*
 - *The angle of ultrasonic refraction at the interface between the pipe wall and the fluid varies with speed of sound in the fluid and affects the flow measurement*
 - *Claims include*
 - *Measurement of the speed of sound in the fluid can be used to compensate the flow measurement*

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Supplier Claims

- *Dimensional Uncertainty*
 - *Claims include*
 - *Spool construction are superior to clamp-on designs because their geometry is known and can be wet tested*

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Supplier Claims

- *Shear Mode vs. Axial Beam*
 - *Shear mode beams typically take the shape of a cylinder between the sensors*
 - *Axial mode beams travel downstream within the pipe wall continually releasing a wide coherent beam of ultrasonic energy into the fluid*

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Supplier Claims

- *Shear Mode vs. Axial Beam*

- *Claims include*

- *Changing velocity causes shear beams to move relative to the receiving sensor and affect the measurement*
 - *Excessively high velocity could cause shear beams to miss the receiving sensor*

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Supplier Claims

- *Shear Mode vs. Axial Beam*

- *Claims include*

- *Axial beams (that are wider) will not shift away from the sensor*
 - *Axial beams (that are coherent) generate a stronger signal that is less susceptible to blockage by vapors in liquid service and moisture in gas service*

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Supplier Claims

- *Zero Drift Correction*

- *Claims include*

- *Comparison of axial beam transit time measurements in the fluid and in the pipe wall can be used to constantly correct for zero drift while the fluid is flowing*

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Supplier Claims

- *Accurate Time Measurement*
 - *Claims include*
 - *Accurate time measurement results in better flow measurement, especially in smaller pipes and at low flow rates*

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Seminar Outline

- *Introduction*
- *Fluid Flow Fundamentals*
- *Flowmeter Technology*
- *Flowmeter Performance*
- *Consumer Guide*

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Consumer Guide

User Equipment Selection Process

- *Learn about the technology*
- *Find suitable vendors*
- *Obtain specifications*
- *Organize specifications*
- *Evaluate specifications*
- *Select equipment*

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Consumer Guide

User Equipment Selection Process

- *Performing this process takes time and therefore costs money*

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Consumer Guide

User Equipment Selection Process

- *Haphazard implementation with limited knowledge of alternatives does not necessarily lead to a good equipment selection*

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Consumer Guide

Guide Provides First Four Items

- *Learn about the technology*
- *Find suitable vendors*
- *Obtain specifications*
- *Organize specifications*
- *Evaluate specifications*
- *Select equipment*

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Consumer Guide

Guide Provides First Four Items

- **Information focused on technology**
- **Comprehensive lists of suppliers and equipment**

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Consumer Guide

Guide Provides First Four Items

- **Significant specifications**
- **Lists of equipment organized to facilitate evaluation**

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Consumer Guide

User Equipment Selection Process

- **By providing the first four items, the Consumer Guides:**
 - **make technical evaluation and equipment selection easier, more comprehensive, and more efficient**

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Consumer Guide

User Equipment Selection Process

- *By providing the first four items, the Consumer Guides:*
 - *allow selection from a larger number of suppliers*
 - *simplifies the overall selection process*

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Consumer Guide

- ***Supplier Data and Analysis***
- ***Attachments***
 - *Flowmeter categories*
 - *Availability of selected features*
 - *Models grouped by performance*

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Supplier Data and Analysis

- ***Sensor Limits***
 - *Size*
 - *6-10,000+ mm*
 - *Ambient temperature*
 - *-20 to 60°C typical*
 - *Wetted parts*
 - *Clamp-on has no wetted parts*
 - *NEMA 4X, IP65, 67*

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Supplier Data and Analysis

- *Process Operating Limits*
 - *Pressure limit*
 - *Clamp-on has no restrictions*
 - *Temperature limit*
 - *150°C typical; 600°C max*
 - *Composition*
 - *Clamp-on has no restrictions*

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Supplier Data and Analysis

- *Process Operating Limits*
 - *Doppler*
 - *25-100 ppm of 25-100 micron bubbles/suspended solids*
 - *Transit Time*
 - *5 to 50% bubbles by volume (depends on design)*
 - *Suspended solids*

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Supplier Data and Analysis

- *Sensor Installation/Maintenance*
 - *Velocity profile*
 - *10-15D/5D typical*
 - *Condition of inside pipe wall*

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Supplier Data and Analysis

- *Sensor Installation/Maintenance*
 - *Sensor replacement*
 - *Clamp-on*
 - *Probe (wetted)*

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Supplier Data and Analysis

- *Sensor Installation/Maintenance*
 - *Ultrasonic path*
 - *Fluid conductivity*
 - *Quality of reflections (multi-traverse)*
 - *“Quiet” valve trim*

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Supplier Data and Analysis

- *Sensor Installation/Maintenance*
 - *Ultrasonic path*
 - *Sensor corrosion/coating (wetted)*
 - *Sensor coating (wetted)*
 - *Sensor/pipe connection (clamp-on)*
 - *Grease/gel*
 - *RTV*
 - *Epoxy*

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Supplier Data and Analysis

- *Transmitter*
 - *4-wire device (separate power/analog wires)*
 - *Using DC power can eliminate power conduit*
 - *Typically measure forward and reverse flow*
 - *Alarms, totalization, batching*
 - *Multivariable (speed of sound in fluid)*

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Supplier Data and Analysis

- *Transmitter*
 - *Mounting*
 - *Integral*
 - *Remote*
 - *Spacing (distance)*

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Supplier Data and Analysis

- *Transmitter*
 - *Filtering is typically used*
 - *Multiple paths and traverses improve performance*
 - *Signal processing is more complex*
 - *More ultrasonic energy needed*

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Supplier Data and Analysis

- *Transmitter*
 - *Many models do not allow adjustment of full scale*
 - *Range adjustment mechanisms provide insight into age of design*
 - *Analog (potentiometer)*
 - *Dip switch*
 - *Digital*

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Supplier Data and Analysis

- *Performance*
 - *Typically specified in velocity (not flow)*
 - *Specifications are often not clear as to whether the stated accuracy is the*
 - *Reference accuracy*
 - *Theoretical accuracy*
 - *Calibratable accuracy*
 - *Typical installed accuracy*

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Supplier Data and Analysis

- *Performance*
 - *Often assumes known pipe dimensions and pipe conditions*
 - *Performance can vary*
 - *Unmeasured pipe section*
 - *Measured pipe section*
 - *Calibrated spool*

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Supplier Data and Analysis

- *Performance*
 - *Typically based on pulse output*
 - *Analog output accuracy*
 - *Add 0.01% full scale*
 - *Add 0.10% rate plus 0.10% full scale*
 - *Some suppliers could not quantify*

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Supplier Data and Analysis

- *Performance*
 - *It can be difficult to compare the performance of different suppliers' equipment*

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Supplier Data and Analysis

- *Operating Effects*
 - *Ambient*
 - *Temperature, humidity*
 - *Process conditions*
 - *Temperature, pressure, pipe material, composition*
 - *Speed of sound affects angle of refraction between pipe wall and fluid (clamp-on)*

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Supplier Data and Analysis

- *Operating Effects*
 - *It can be difficult to compare the operating effects of different suppliers' equipment*

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Consumer Guide

- *Supplier Data and Analysis*
- **Attachments**
 - *Flowmeter categories*
 - *Availability of selected features*
 - *Models grouped by performance*
 - *Models grouped by supplier*

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Flowmeter Categories

- *Summary of offerings*
 - *Fluid*
 - *Type*
 - *Pipe Material*
 - *Handheld/portable*
 - *Manufacturing location/source*

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Flowmeter Categories

- *Suppliers (74)*
- *Manufacturers (61)*
 - 23 *USA*
 - 8 *Germany*
 - 6 *Japan*
 - 5 *UK*
 - 4 *France, Russia*

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Availability of Selected Features

- *Approvals*
 - *Nuclear feed water*
 - *Custody transfer*
 - *CEMS*

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Availability of Selected Features

- *Transmitter*
 - *Hazardous locations*
 - *Integral, remote*
 - *Housing (NEMA/IP rating)*
 - *Data logging*

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Availability of Selected Features

- *Sensors*
 - *Clamp-on*
 - *Hot tap*
 - *Removable*
 - *Internal*
 - *Housing (NEMA/IP rating)*
 - *Maximum temperature*

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Availability of Selected Features

- *Communications*
 - *HART*
 - *Foundation Fieldbus*
 - *Profibus*

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Models Grouped by Performance

- *Liquid*
 - *Portable and Handheld*
 - *Clamp-on*
 - *Spool*
 - *Probe (wetted)*
- *Gas, Stack Gas, Flare Gas*

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Models Grouped by Supplier

- *Alphabetical listing by supplier*

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Review and Questions

- *Introduction*
- *Fluid Flow Fundamentals*
- *Flowmeter Technology*
- *Flowmeter Performance*
- *Consumer Guide*

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The Consumer Guide to Ultrasonic Flowmeters

*Seminar Presented by
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